



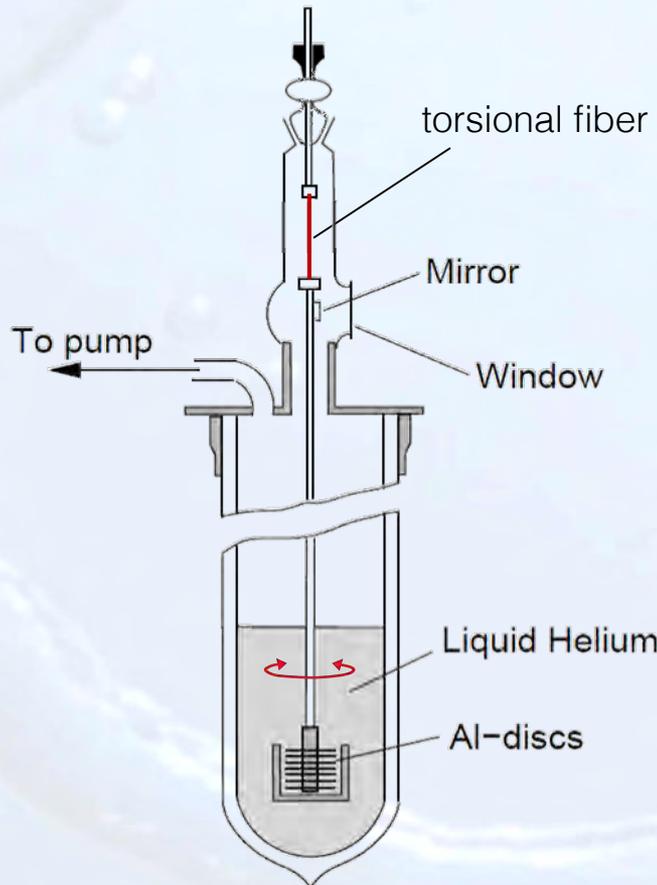
## Determination of $\rho_n$

Experiment of Andronikasvili (1948)

First **direct** observation of  $\rho_n$



Elepter Luarsabovich  
Andronikashvili (1910-1989)



**50 aluminum discs**

thickness 13  $\mu\text{m}$

diameter 3.5 cm

spacing 210  $\mu\text{m}$

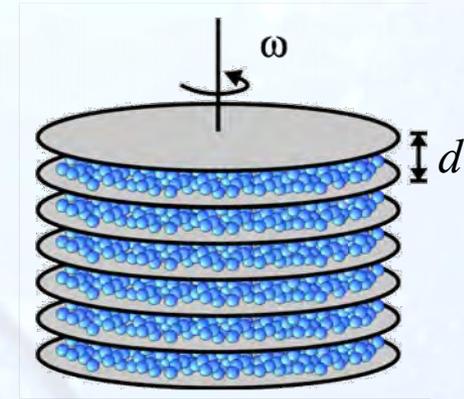


observation  $\rightarrow$  slow resonant oscillations (mass and torsion fiber)

Important parameter is the viscos penetration depth for wave with frequency  $\omega$

$$\delta = \sqrt{2\eta_n / \rho_n \omega}$$

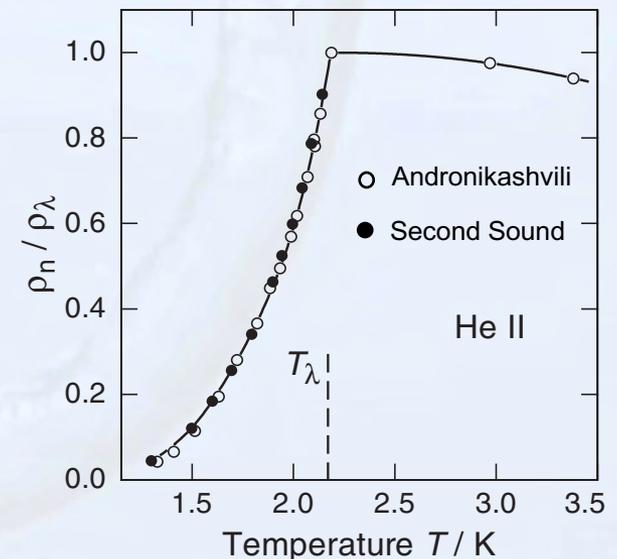
- $d < \delta$ :
- $\blacktriangleright$   $\rho_n$  is dragged along with torsion oscillator above and below  $T_\lambda$
  - $\blacktriangleright$   $\rho_s$  remains stationary
  - $\blacktriangleright$  period of oscillation determined by mass of torsion oscillator (and spring constant)
- $\rightarrow$   $\rho_n$  can be determined



temperature dependence (empirical relation)

$$\rho_n = \rho_\lambda \left( \frac{T}{T_\lambda} \right)^{5.6}$$

comparison with 2<sup>nd</sup> Sound  $\rightarrow$  fits well





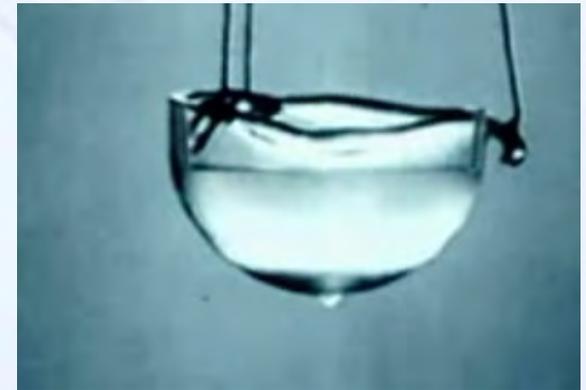
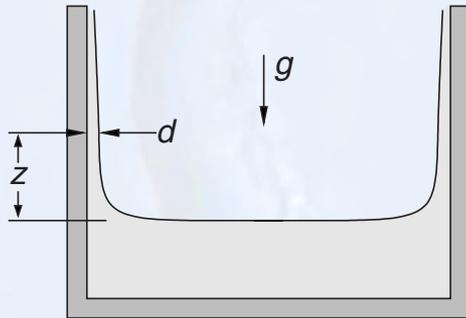
## b) Beaker experiments

**films** are formed with a **thickness** of  $\sim 200 \text{ \AA}$  in saturated vapor pressure also **against gravity**

let us understand how

comment: the film formation is a “classical” phenomenon

### (i) Film formation in saturated vapor



In thermal equilibrium

$$\mu_f = \mu_g = \mu_l$$

↙ chemical potential for film (gas and liquid)

gravitational force is compensated by v. Waals forces

$$\rightarrow \mu_f = \mu_l + \underbrace{\mu_{\text{grav}} + \mu_{\text{vdW}}}_{=0} = \mu_l$$



film thickness:

$$\mu_{\text{grav}} = gz$$

$$\mu_{\text{vdW}} = -\alpha/d^3$$

$$\left. \begin{array}{l} \mu_{\text{grav}} = gz \\ \mu_{\text{vdW}} = -\alpha/d^3 \end{array} \right\} gz - \alpha/d^3 = 0 \quad \curvearrowright$$

$$d = \sqrt[3]{\frac{\alpha}{gz}}$$

depends on film thickness:  $\mu_{\text{vdW}} = -\alpha/d^3$  for  $d < 30 \text{ nm}$

$\mu_{\text{vdW}} = -\alpha/d^4$  for  $d > 80 \text{ nm}$

atomic polarisability of helium + wall  
(Hamaker constant)

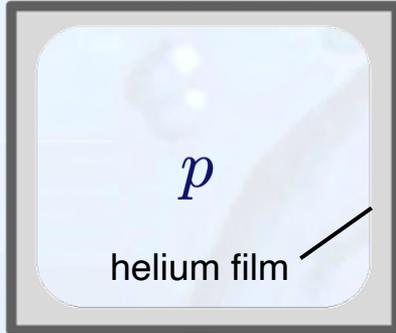
retardation of potential

typical value:  $d \sim 20 \text{ nm}$  at  $z = 10 \text{ cm}$

comment: property of **superfluidity** is **unimportant** for the **film formation** and **thickness**, but for the film flow



### (ii) film formation in unsaturated vapor



How does  $d$  depend on  $p$  ?

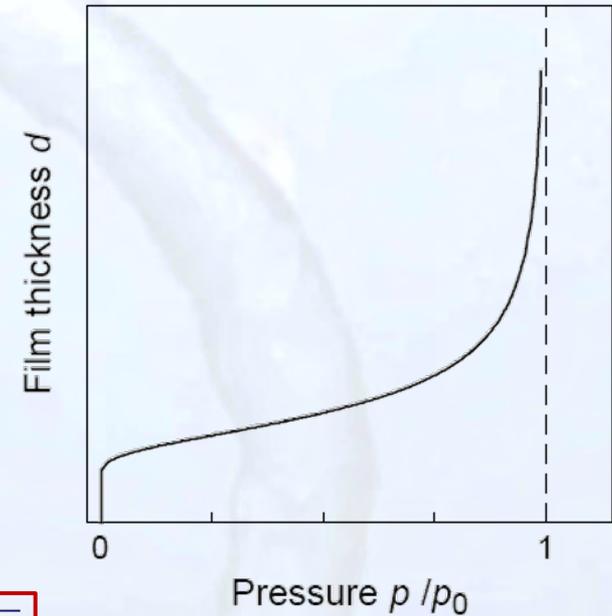
→ barometric formula

$$\frac{p}{p_0} = e^{-mgh/k_B T}$$

$$mgh = k_B T \ln \left( \frac{p}{p_0} \right)$$

→ 
$$\frac{\alpha}{d^3} = \frac{k_B T}{m_4} \ln \left( \frac{p_0}{p} \right)$$

→ 
$$d = \sqrt[3]{\frac{\alpha m_4}{k_B T (\ln p_0 - \ln p)}}$$



- ▶ decrease of pressure → decrease of film thickness
- ▶ in practice: thinknesses of **sub-mono layers** are possible and realized

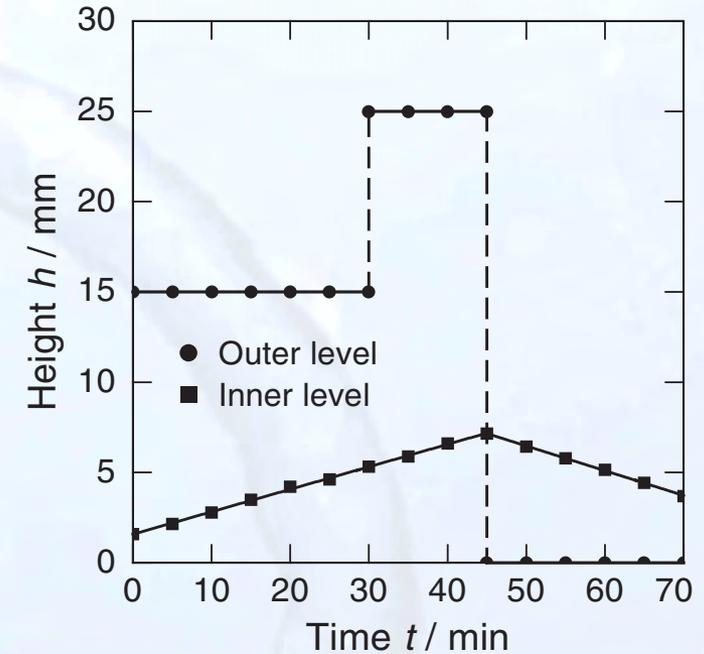


investigation of superfluidity with **third sound**: **onset of superfluidity** at  $n > 2.1$  layers



now back to the film flow:

- ▶ films are formed
- ▶  $\rho_s$  is moving without friction
- ▶ equalizing the chemical potential is driving force
- ▶ const. rate  $\triangleq$  critical velocity



Interesting question:  $\rho_s$  flows with  $S = 0$ !  $\rightarrow$  rest should warm up and helium flowing into a vessel should have  $T = 0$ !

but thermal equilibrium via gas phase



density  $\rho = \rho_n + \rho_s$  (1)

mass flow  $\mathbf{j} = \rho_n \mathbf{v}_n + \rho_s \mathbf{v}_s$  (2)

mass conservation  
continuity eqn.  $\frac{\partial \rho}{\partial t} = -\text{div } \mathbf{j}$  (3)

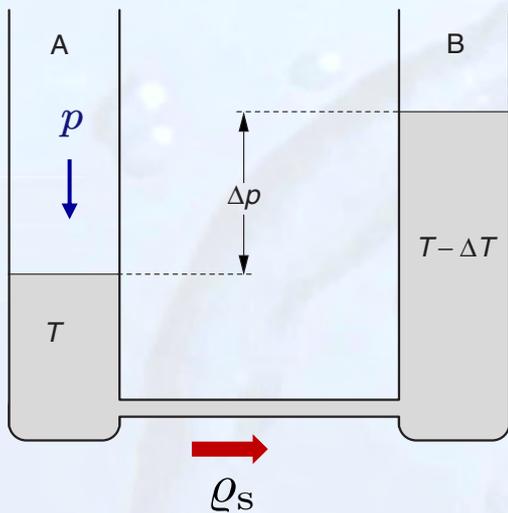
ideal fluid  $\frac{\partial \mathbf{j}}{\partial t} = -\text{grad } p$  (4)

entropy conservation  $\frac{\partial(\rho S)}{\partial t} = -\text{div}(\rho S \mathbf{v}_n)$  (5)

an equation of motion for  
superfluid component  $\frac{\partial \mathbf{v}_s}{\partial t} = S \text{ grad } T - \frac{1}{\rho} \text{ grad } p$  (6)

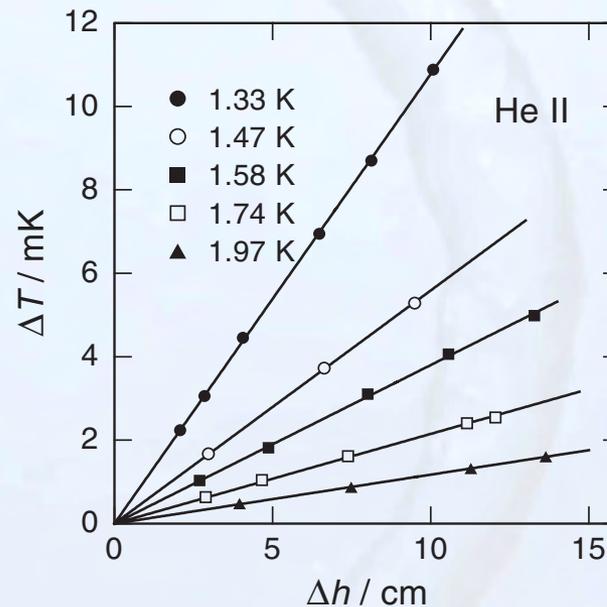


## c) Thermomechanical effect



$+ Q_s$   $\rightarrow$  cooling in B  
 $- Q_s$   $\rightarrow$  warming in A

$T_B < T_A$



Using (6) in stationary state

$$\frac{\partial v_s}{\partial t} = S \text{grad } T - \frac{1}{\rho} \text{grad } p = 0$$

$\uparrow$   
 in equilibrium **nothing flows**

$$\frac{\Delta p}{\Delta T} = \rho S$$

London equation  
(H. London 1939)

$\rightarrow$  Linear relation between  $\Delta p$  and  $\Delta T$

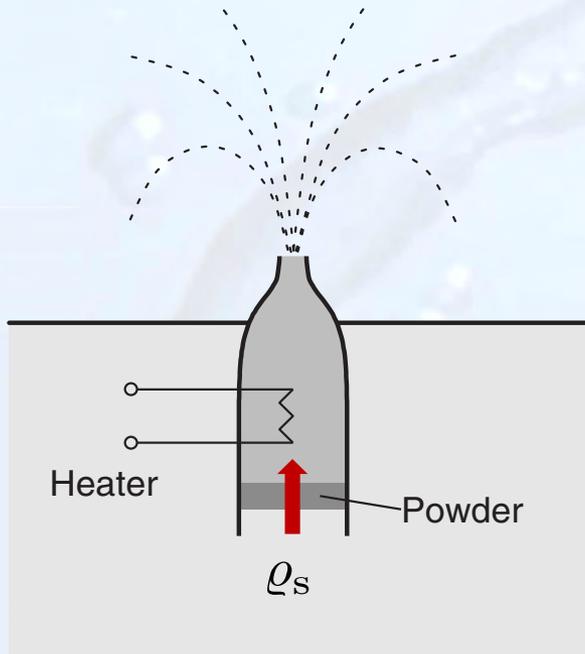
$\Delta h = 2 \text{ cm}$   
 $T = 1.5 \text{ K}$

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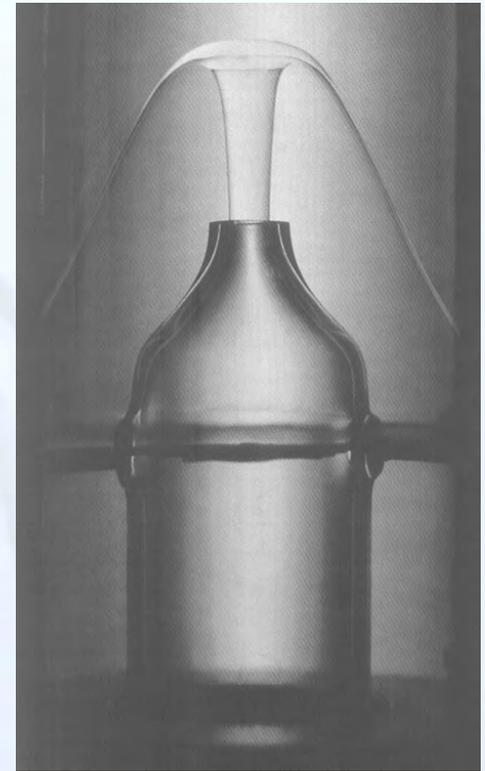
$\Delta T = 1 \text{ mK}$       not very effective cooling



### Reverse thermomechanical effect: Fountain effect



$$\Delta T \quad \curvearrowright \quad \Delta p$$



- ▶ heating of helium inside vessel  $\rightarrow$  ratio of  $\rho_n/\rho_s$  increases inside the vessel
- ▶ the temperature inside is higher than outside
- ▶ to equalize the system  $\rho_s$  flows through superleak (compressed powder)
- ▶ pressure rises and fountain starts to flow (and flows as long as heater is on)



### d) Heat Transport

- ▶ in not too small capillaries  $v_n \neq 0$
- ▶ even in equilibrium ( $\Delta p = \rho S \Delta T$ ) there is a constant flow of  $\varrho_n$  from the warm end to the cold end and  $\varrho_s$  in the opposite direction by “convection”

$$\left. \begin{array}{l} \varrho_n \longrightarrow \text{cold end} \\ \varrho_s \longrightarrow \text{warm end} \end{array} \right\} \text{entropy transport} \triangleq \text{heat transport}$$

heat transport maximum at 1.8 K where  $\varrho_n \approx \varrho_s$

- ▶ limited only by the mobility of  $\varrho_n$  and therefore  $\eta_n$
- ▶ viscos mass flow of  $\varrho_n$  :

volume rate  $\dot{V}_n = \frac{\beta}{\eta_n} \frac{\Delta p}{L}$

(\*)

$$\begin{array}{l} \beta \propto r^4 \quad \text{for capillaries} \\ \beta \propto d^3 \quad \text{for slits} \end{array}$$

- ▶ entropy flow  $\dot{V}_n \varrho S$   $\longrightarrow$  heat flow  $\dot{Q} = T \dot{V}_n \varrho S$  (\*\*)

$$\delta Q = T \delta S$$



(\*) insert in (\*\*) and London equation ( $\Delta p = \rho S \Delta T$ )

$$\dot{Q} = \frac{\beta T (\rho S)^2}{\eta_n L} \Delta T$$

linear regime

experimental results:

$$\dot{Q} \propto \beta \propto d^3 \quad (\text{as expected})$$

$$\dot{Q} \text{ rises with } T \quad (\text{as expected})$$

heat flow  $\log \dot{Q}/\Delta T$  vs  $\log d$

